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## Amendments to the Claims:

 (Previously Presented) A method of producing xylose from a cellulose material containing hemicellulose, comprising:

providing a pre-hydrolyzed cellulose pulp that is at least partially bleached and has a hemicellulose content that is predominantly xylan;

extracting the hemicellulose from the at least partially bleached pulp into a caustic solution thereby forming a hemicaustic solution:

separating the hemicaustic solution into a concentrated hemicellulose solution and a concentrated caustic solution; and,

hydrolyzing the hemicellulose from the concentrated hemicellulose solution to produce xylose.

- (Original) The method of claim 1, wherein the step of providing pulp comprises
  providing hardwood pulp wherein the pulp is greater than 4 wt% hemicellulose.
- (Original) The method of claim 1, wherein the step of providing pulp comprises providing hardwood pulp where the hemicellulose is greater than 85 wt% xylan.
- 4. (Original) The method of claim 1, wherein the step of providing the at least partially bleached the pulp comprises providing a cooked cellulose pulp and subjecting the cooked pulp to a series of oxidation and extraction stages until greater than 80 wt% of the original lignin content of the pulp has been removed.
- 5. (Previously Presented) The method of claim 1, wherein the step of proving the at least partially bleached pulp comprises providing a cooked cellulose pulp and subjecting the cooked pulp to a series of oxidation and extraction stages until the pulp has an ISO brightness of 88% or higher.
- (Original) The method of claim 1, wherein the step of extracting the hemicellulose from the pulp comprises extracting the hemicellulose using a cold caustic treatment.

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7. (Original) The method of claim 6, wherein the pulp has a consistency of about 2 wt% to about 50 wt% with respect to the caustic solution during cold caustic treatment.

- (Original) The method of claim 7, wherein the caustic solution has a pH greater than 13 during treatment.
- (Original) The method of claim 8, wherein a temperature of the caustic solution is from about 20°C to about 50°C during treatment.
- 10. (Original) The method of claim 6, wherein the cold caustic treatment is continued until the treated pulp contains no more than 15 wt% hemicellulose.
- (Original) The method of claim 10, wherein the cold caustic treatment is continued until the treated pulp contains no more than 5 wt% hemicellulose.
- 12. (Original) The method of claim 1, wherein the step of extracting the hemicellulose from the pulp into a caustic solution comprises holding the pulp in the caustic solution for a period of time and thereafter washing the pulp with water, wherein the caustic solution, extracted hemicellulose, and wash water form the hemicaustic solution.
- 13. (Original) The method of claim 1, wherein the step of separating the hemicaustic solution into a concentrated hemicellulose solution and a concentrated caustic solution comprises subjecting the hemicaustic solution to a separation technique selected from the group consisting of nanofiltration, distillation, centrifugation, and precipitation.
- 14. (Original) The method of claim 13, wherein the step of separating the hemicaustic solution comprises filtering the solution through a nanofiltration apparatus wherein the permeate stream exiting the nanofiltration apparatus is the concentrated caustic solution having greater than about 80 wt% of the original caustic solution, and wherein the concentrate stream is the concentrated hemicellulose solution that constitutes from about 5 wt% to about 30 wt% hemicellulose.

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15. (Original) The method of claim 1, wherein the step of hydrolyzing the hemicellulose from the concentrated hemicellulose solution comprises

acidifying the concentrated hemicellulose solution with a mineral acid; and, acid hydrolyzing the hemicellulose, whereby the xylan content of the hemicellulose is

acid hydrolyzing the hemicellulose, whereby the xylan content of the hemicellulose is converted to xylose.

- 16. (Previously Presented) The method of claim 15, further comprising the step of demineralizing the acidified concentrated hemicellulose solution prior to the acid hydrolyzing step.
- (Original) The method of claim 16, wherein the step of demineralizing is accomplished by filtration.
- (Original) The method of claim 15, further comprising the step of demineralizing the concentrated hemicellulose solution prior to the acidifying step.
- (Original) The method of claim 18, wherein the step of demineralizing is accomplished by ion exchange.
- (Original) The method of claim 15, further comprising the step of removing organic/inorganic acids, metal salts, and colored by-products from the hydrolyzed hemicellulose.
- 21. (Original) The method of claim 20, wherein the step of removing acids, salts, and by-products from the hydrolyzed hemicellulose comprises contacting the hydrolyzed hemicellulose with a cationic ion exchange resin.
- 22. (Original) The method of claim 20, wherein the step of removing acids, salts, and by-products from the hydrolyzed hemicellulose comprises contacting the hydrolyzed hemicellulose with an anionic ion exchange resin.
- (Original) The method of claim 1, wherein the resulting hydrolyzed hemicellulose has a xylose content of greater than 90 wt%.

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(Original) The method of claim 1, wherein the step of providing a pulp comprises
providing a hardwood selected from sweet gum, black gum, maple, oak, eucalyptus,
poplar, beech, aspen, and mixtures thereof;

digesting the hardwood to a hardwood pulp; and, at least partially bleaching the digested pulp.

25. (Previously Presented) The method of claim 1, wherein the step of providing a pulp comprises

pre-hydrolyzing a hardwood feed material;

digesting the pre-hydrolyzed hardwood; and,

at least partially bleaching the digested pulp using a conventional pulp bleaching process.

26. (Previously Presented) A xylose production system comprising a supply of at least partially bleached pre-hydrolyzed cellulose pulp having a hemicellulose content that is greater than 85 wt% xylan;

an alkaline treatment system capable of extracting hemicellulose from the bleached pulp into a hemicaustic solution:

a separation system capable of separating the hemicaustic solution into a purified concentrated caustic solution and a concentrated hemicellulose solution; and,

a hydrolysis unit capable of hydrolyzing the xylan content of the concentrated hemicellulose solution to xylose.

- 27. (Original) The xylose production system of claim 26, further comprising a chemical bleaching operation capable of providing the supply of at least partially bleached cellulose pulp by reducing the lignin content of a cooked hardwood pulp.
- (Original) The xylose production system of claim 27, wherein the alkaline treatment system comprises:

a cellulose slurry supply system for providing the pulp containing hemicellulose to said alkaline treatment system;

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a steeping liquor supply system for providing an effective amount of a caustic steeping liquor comprising an alkaline solution to said alkaline treatment system;

a mixing system for combining the pulp and the steeping liquor into an alkaline cellulose slurry:

at least one alkaline treatment unit for steeping the alkaline cellulose slurry for a sufficient amount of time to diffuse an effective amount of the hemicellulose out of the pulp fibers and into the steeping liquor thereby forming a hemicaustic solution; and,

at least one treated cellulose washer to separate the hemicaustic solution from the treated cellulosic fibers.

- (Original) The xylose production system of claim 28, wherein the steeping liquor supply system further comprises at least one chiller.
- (Original) The xylose production system of claim 26, wherein the separation system is a nanofiltration system.
- 31. (Previously Presented) The xylose production system of claim 30, wherein said nanofiltration system includes at least one nanofiltration membrane capable of excluding compounds having a molecular weight of about 200 Daltons and higher.
- (Original) The xylose production system of claim 31, wherein said nanofiltration system comprises a plurality of nanofiltration units.
- (Original) The xylose production system of claim 32, wherein said nanofiltration system further comprises an evaporation system.
- (Original) The xylose production system of claim 26, wherein the hydrolysis unit comprises:
  - a demineralization stage for reducing alkali content of the hemicellulose solution; an acidification stage for introducing a mineral acid to the hemicellulose solution; and, a hydrolysis reactor to hydrolyze hemicellulose.

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35. (Currently Amended) A process for producing a xylose product from a cellulose material, comprising the steps of:

at least partially chemically bleaching a cooked <u>pre-hydrolized</u> cellulose pulp using a conventional pulp bleaching process;

using a cold caustic treatment to extract hemicellulose from the at least partially bleached cellulose pulp into a caustic solution thereby forming a hemicaustic solution;

separating the hemicaustic solution by nanofiltration into a concentrated hemicellulose solution and a concentrated caustic solution; and,

hydrolyzing the hemicellulose from the concentrated hemicellulose solution.

- 36. (Original) The process of claim 35, wherein the step of providing a cellulose pulp comprises providing a hardwood pulp wherein the hardwood is greater than 5 wt% hemicellulose.
- 37. (Original) The process of claim 36, wherein the hemicellulose of the hardwood is greater than 85 wt% xylan.
- 38. (Previously Presented) The process of claim 35, wherein the at least partially bleached pulp has an ISO brightness of 88% or higher.
- 39. (Original) The process of claim 35, wherein the cold caustic treatment is continued until the treated pulp contains no more than 15 wt% hemicellulose.
- (Original) The process of claim 39, wherein the cold caustic treatment is continued until the treated pulp contains no more than 5 wt% hemicellulose.
- 41. (Original) The process of claim 35, wherein the step of nanofiltering the hemicaustic solution comprises filtering the solution through a nanofiltration apparatus wherein the permeate stream exiting the nanofiltration apparatus is the concentrated caustic solution having greater than about 80 wt% of the original caustic solution, and wherein the concentrate

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stream is the concentrated hemicellulose solution that constitutes from about 5 wt% to about 30 wt% hemicellulose.

42. (Original) The process of claim 35, wherein the step of hydrolyzing the hemicellulose from the concentrated hemicellulose solution comprises

neutralizing the concentrated hemicellulose solution with a mineral acid; and, acid hydrolyzing the hemicellulose, whereby the xylan content of the hemicellulose is converted to xylose.

- (Previously Presented) The method of claim 35, further comprising the step of acidifying the concentrated hemicellulose solution prior to the hydrolyzing step.
- (Previously Presented) The method of claim 42, further comprising the step of demineralizing the concentrated hemicellulose solution prior to the acid hydrolyzing step.
- (Original) The process of claim 42, further comprising the step of removing organic/inorganic acids, metal salts, and colored by-products from the hydrolyzed hemicellulose.
- 46. (Original) The process of claim 35, wherein the resulting hydrolyzed hemicellulose has a xylose content of greater than 90 wt%.
- (Previously Presented) The method of claim 6, wherein a temperature of the caustic solution is less than 50°C during treatment.
- 48. (Previously Presented) A method of producing xylose from a cellulose material containing hemicellulose, comprising:

providing a cellulose pulp that is at least partially bleached and has a hemicellulose content that is predominantly xylan;

extracting the hemicellulose from the at least partially bleached pulp into a caustic solution thereby forming a hemicaustic solution:

separating the hemicaustic solution into a concentrated hemicellulose solution and a concentrated caustic solution; and,

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hydrolyzing the hemicellulose from the concentrated hemicellulose solution to produce a xylose product having a purity of 80 wt% or greater in the absence of an additional purification step.